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CHARACTERIZATION AND GRAVITY SEPARATION OF NONSULFIDE ZINC DEPOSITS FROM UM GHEIG MINE, RED SEA COAST, EGYPT

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This paper aims to beneficiation of Um Gheig nonsulfide Zinc ore from its associated gangues using the gravity separation "shaking table" technique. The different operating parameters affecting of the efficiency of the separation process is evaluated.

The zinc locality of Um Gheig represents one of the important nonsulfide zinc deposits along the coastal plain of the Red Sea Coast, Egypt. These zinc ores are called "calamines" and consist mainly of a mixture of zinc carbonates (smithsonite, hydrozincite) and zinc silicates (hemimorphite), with a variable content of calcite, goethite and Pb bearing minerals.

Extensive mineralogical (using XRD, XRF) and petrographic studies have been carried out on the selected samples from Um Gheig Mine. Theses investigations show that, the nonsulfides mineral association in the deposit consists mainly of smithsonite (50.74%), hydrozincite (18.78%) and hemimorphite (14.78%) replacing both primary ore minerals and carbonate host rocks. Smithsonite occurs in two generations, cryptocrystalline mixed with goethite and rhombohedral crystals, precipitate in vugs and open space of the high grade ore. The main gangue minerals are calcite and goethite. XRF analysis indicates that the sample contains 47.50% ZnO, 1.55% PbO and about 29.28% L.O.I.

Liberation and mineralogical investigation showed that higher degree of liberation (over 90%) between the valuable zinc bearing minerals and their gangues can be achieved below the size 0.106 mm.

The results of gravity separation showed that the best operating parameters to obtain a concentrate with high assay and recovery are at inclination angle (4 degree), stroke length (2.5 cm), feed rate (150 gm / min), and water flow rate (25 l / min). At these optimum conditions a concentrate assaying 60.85 % ZnO was obtained with a recovery of ~90 %.

KEYWORDS: Nonsulfide zinc ore, Mineralogy, Petrography, Liberation size, Gravity separation, Shaking table

1. INTRODUCTION

The area of Um Gheig mine is a part of the coastal plain of the Red Sea Coast, Egypt. It lies 38 km south of Quseir City (Fig.1). The area can be reached by Quseir-Mersa

Alam asphalet road. The Um Gheig mine is located in Wadi Um Gheig, 7.5 km from the west of the Quseir -Mersa Alam asphaletic road.

Um Gheig ore is a nonsulfide Zn (Pb) deposit with estimated reserves of about two million ton with an average grade of 10% Zn, 2% Pb [1,2]. The definition of "Nonsulfide zinc" is a very general term, which comprises a large series of minerals [2-4]. The only minerals of current economic importance are ; the carbonates smithsonite and hydrozincite, and the silicates hemimorphite, willemite, as well as Zn smectite. The economic value of zinc nonsulfide ores is thus dependent not only on the geologic setting of each deposit but also on the specific characteristics of the mineralogical association and the nature of the gangue minerals [4-6].

Within the last decade, with the development of solvent-extraction and electro-winning processes for the treatment of nonsulfide zinc ores, there has been a renewed commercial interest for this type of mineralization throughout the world [2,3,7]. The commercial exploitation of nonsulfide deposits, commonly defined as "Zinc Oxides" or "Calamine" (nonsulfide Zn ore in carbonate rocks), is rapidly becoming an important source of metallic zinc. Moreover, it is expected that in the near future the annual production of zinc from these ores could exceed 10% of the global zinc metal production. Scientific researches is now focused not only on several economic "Zinc Oxide" deposits throughout the world [2,8-10] but also on older mining districts containing smaller and historically exploited deposits [11-13]. Compared to sulfide deposits, their main attraction lies in: a) their distinct scarcity or lack of Pb, S and other undesirable elements, b) their relatively low-energy recovery by solvent extraction and electro-winning and c) the generation of higher economic value on site.

A wide series of papers focused on the traditional treatment of nonsulfides (including flotation processes), spanning the first seventy years of the last century [14-16]. On the contrary, there are not as many recent published studies on the hydrometallurgical behavior of nonsulfide Zn minerals [6,17-20], because most mining companies are still in the experimentation phase.

The main goal of the present study is to separate the nonsulfide zinc from its associated gangues of Um Gheig mine through several beneficiation steps comprised of mineralogical investigation, liberation study and gravity separation by "shaking table".

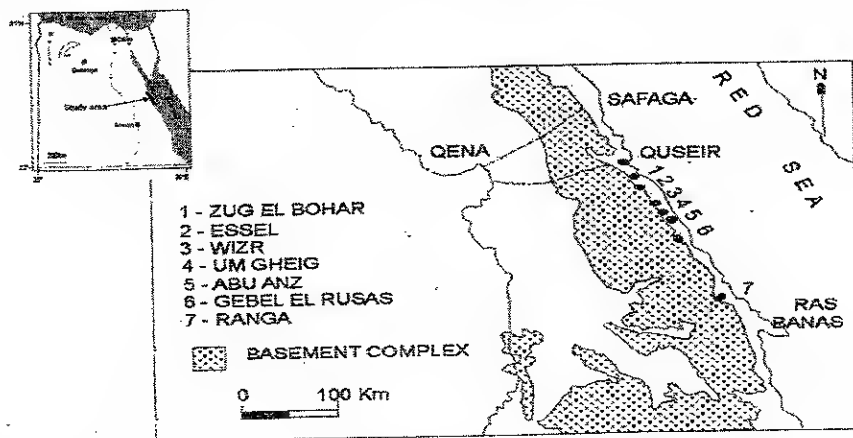


Fig.1. Location Map of the Zinc occurrences along the Red Sea coastal zone, Egypt.

2. EXPERIMENTAL WORK

2.1. Sample Preparation and Characterization

A representative sample from Um Gheig mine, Egypt, was subjected to crushing by a "Denver" jaw crusher. Then the sample was divided into equal batches using coning and quartering method. One of these batches was further representatively divided into batches each of 5 kg weight. One of the latter was further sampled into 250g batches using "Jones Riffle" sampler. A sample of them was ground and subjected for complete chemical analysis by X-ray fluorescence and X-ray diffraction as well as mineralogical analysis. Also ore preparation processes involved attrition scrubbing of the crushed ore to remove the dust and clay from the surface of the particles. Wet-dry size analysis using a series of ASTM standard sieves (i.e. 4, 3.327, 2.36, 1.16, 0.833, 0.589, 0.417, 0.298, 0.208, 0.106, 0.071, and 0.036 mm) was performed. After screening, each size fraction was collected, weighed, and chemically analyzed for ZnO %. The degree of liberation was investigated, by using optical microscope; where each size fractions of mineral particles were mounted on thin sections and, later on, analyzed by optical microscope.

2.2. Shaking Table Experiments

A "Wilfley" shaking table was used in this study, Figure (2). Four parameters are studied; namely; inclination angle, stroke length, feed rate and water flow rate. The experiments were carried out at feed particle size $-0.125 + 0.08$ mm, which represent about 59.37% of the feed sample, where maximum liberation can be attained.

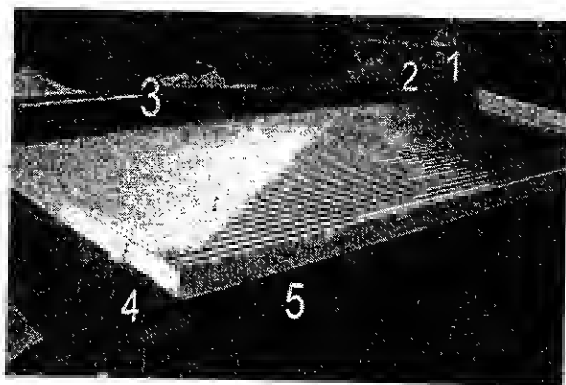


Fig. (2) Wilfley Shaking Table Unit
1: Sample feeding box, 2: Washing water feeding box, 3: Washing water, 4: Heavy products reservoirs, 5: Light products reservoirs

3. RESULTS AND DISCUSSION

3.1. Sample Preparation

Table (1) gives the results of the wet and dry size analysis of the representative sample whereas Table (2) gives the results of size and mineralogical analyses of its attrition scrubbed product. These results show the ore is generally friable in nature where it was noted that about 40.63% of the ore passed through the sieve -0.036 mm after attrition scrubbing process. Mineralogical analysis (Table 2) indicated that most of such finest size fraction (-0.036 mm) is composed of hydrozincite due to the friability of hydrozincite in comparison to the other forms of zinc minerals and in turn most of

hydrozincite rapidly affected by crushing and grinding processes than the other non-sulphide minerals.

Table (1): The results of the wet and dry size analysis of the sample

Size (mm)	Dry analysis	Wet analysis
	Cum weight%	Cum weight%
-0.036	4.14	5.81
0.036	5.71	6.66
0.071	7.22	8.29
0.106	9.78	9.93
0.208	11.96	11.49
0.295	14.76	13.70
0.417	18.38	16.35
0.589	22.55	19.74
0.833	27.72	24.63
1.168	42.25	39.26
2.36	56.26	53.89
3.327	69.22	63.36
+4.00	100	100

Table (2) Size and mineralogical analyses of attrition scrubbing product

Size, mm	Weight %	Minerals %				
		Smithsonite	Hydrozincite	Hemimorphite	Calcite	Goethite
Bulk	100	54.60	19.22	12.76	10.72	2.82
+0.2	54.81	63.35	10.58	12.64	10.81	2.64
-0.2 + 0.1	1.70	36.00	8.48	39.38	13.28	2.88
-0.1 + 0.036	2.88	23.66	6.64	44.54	26.57	3.11
-0.036	40.63	30.55	56.26	2.84	6.35	4.01

3.2. Characterization of Nonsulfide Zinc Ores

Identification and characterization of minerals is of fundamental importance in the development and operation of mining and mineral processing systems [21], and it is very important in designing a suitable flow sheet for recovering the valuable metals. It is also critical in optimizing actual plant for improving performance [22]. The X-ray diffraction (XRD), chemical analysis, liberation study, and mineralogical investigation were used to determine the main zinc components of the ore and their associated gangues as well as the liberation degree which significantly affect the separation results in terms of grade and recovery. Table (3) gives the mineralogical and chemical composition of the non-sulphide zinc minerals and their associated gangue minerals. It shows that smithsonite is the major non-sulphide Zinc minerals where it represents about 50.74 % by weight, whereas hydrozincite and hemimorphite represent 18.78 %

and 14.78 % respectively. On the other hand calcite is the major gangue minerals (15.78 % in weight) and goethite (2.86 %), as showed in Table (3). This is also confirmed from the results of chemical analysis of the sample as shown in Table 3. The sample contains about 47.5 % ZnO, 29.33 % LOI, 8.0 % CaO, 4.34 % SiO₂, 4.07 % Fe₂O₃ and lower amount (1.55 %) of PbO.

Table (3) The Mineralogical and chemical composition of the representative sample.

representative sample.										
Mineralogical composition %										
smithsonite	hydrozincite	hemimorphite	Calcite	Goethite	Halite	Quartz				
50.74	18.78	14.78	15.72	2.86	0.48	1.03				
Chemical composition %										
ZnO	PbO	CaO	Fe ₂ O ₃	SiO ₂	MnO	SO ₃	Cl	Na ₂ O	MgO	L.O.I
47.50	1.55	8.01	4.07	4.34	1.03	0.56	2.01	0.36	0.56	29.33
L.O.I = loss on ignition at 1100°C										

L.O.I= loss on ignition at 1100° C

There are two generations of smithsonite recognized under the polarized microscope and SEM. Smithsonite that occurs as dull, cryptocrystalline with no visible crystals (Fig. 3a). The second smithsonite generation (late smithsonite) occurs as clear rhombohedral crystals, precipitate in vugs and open space of the high grade ore (Fig. 4a). Hydrozincite occurs in different generations in the samples, the first hydrozincite generation occurs as veins growing in smithsonite; veins occur as thin, small veins (Fig. 3b), hydrozincite also occurs as nodules growing in the cavities between smithsonite (Fig. 3c) and botryoidal hydrozincite (4b). Two hemimorphite generations could be observed. The first generation occurs as small concretions growing in fine-grained smithsonite (Fig. 3d). The second one appears as clear elongated crystals growing in veins and cavities (Fig. 3e). Calcite associated with supergene Zn-Pb mineralization is relatively common, with crystals filling the vugs and open space in several samples (Fig. 3f), and also found as precipitate on the mineral surface.

Measurement of the degree of liberation of the minerals, a property directly related to the particle composition distribution as a function of particle size, was an extremely complex problem. Based on processing of optical or SEM images (back scattered electrons or X-ray spectra) are becoming faster and more efficient.

In this study, each size fractions of mineral particles were mounted on thin sections and, later on, analyzed by optical microscope. To achieve relatively high grades and recoveries in mineral processing; the valuable mineral must be individualized to almost mono-mineral particles by grinding operations prior to the physical concentration process.

Figures 5a and 5b show complex interlocking and growth between non-sulphide Zn minerals (smithsonite, hydrozincite and hemimorphite) and calcite gangue minerals. Fig 5c shows that interlocking between non-sulphide Zn minerals and calcite is less complex "ternary particle". Fig 5d show that the grain boundaries of smithsonite, hydrozincite, hemimorphite and calcite have little interpenetration (usually binary interlocking), Figs 5e and 5f show that about more than of 90% fraction of the valuable non-sulphide Zn minerals (liberated) to consider a particle as "free".

Higher degree of mineral liberation ($>90\%$) was attained at 0.106 mm, as individual component minerals were distinctly separated. This was taken into consideration in preparing the feed samples for beneficiation experiments.

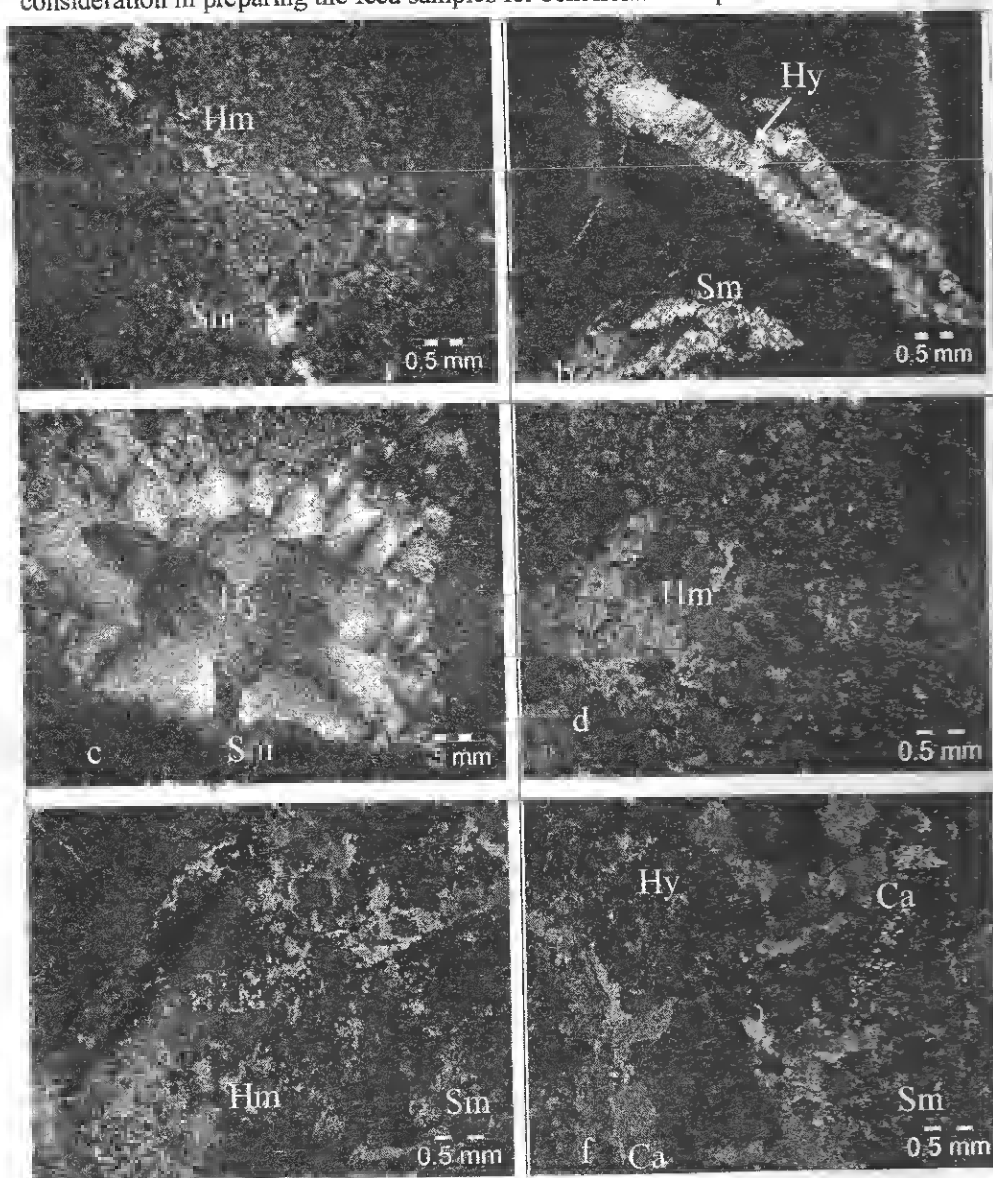


Fig.3. a) Smithsonite (sm) fine ground mass, cryptocrystalline, with no visible crystals. b) Hydrozincite (Hy) veins growing in smithsonite mixed with iron oxide. c) Hydrozincite nodules growing in smithsonite. Note that, hydrozincite grade from fine small crystals to large hydrozincite crystals. d) hemimorphite (Hm) with a dusty appearance inter growing in fine grained smithsonite.(first generation). e) Elongate hemimorphite veins growing in open space between smithsonite. (Second generation). f) Calcite (Ca) precipitate and filling in the vugs and open space.

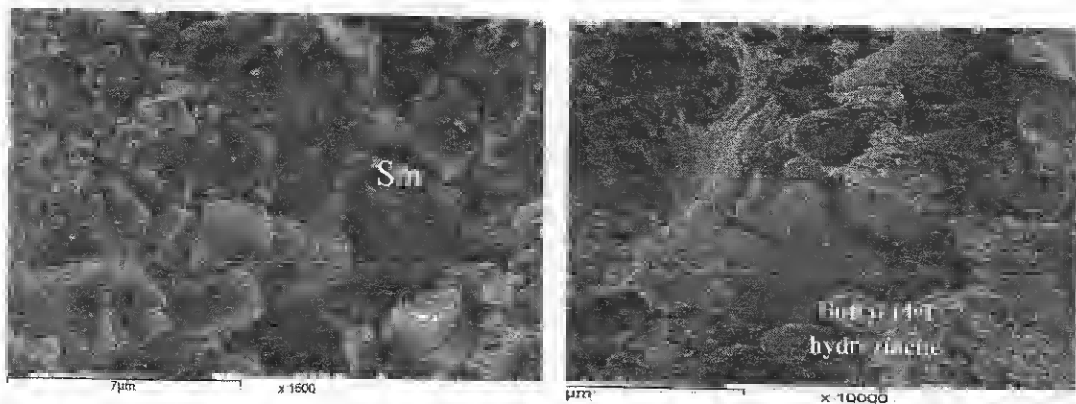


Fig4. SEM of samples from Um Gheig nonsulfide deposits. a) Rhombohedra crystals of smithsonite (sm), filling vugs and open space of high grade ore sample. b) Botryoidal hydrozincite (Hy) in cavities between smithsonite.

3.3. Shaking Table Separation Results

Due to the difference in specific gravity between non-sulphide Zinc minerals (smithsonite, hydrozincite and hemimorphite with sp.gr of 3.5 to 4.5) and the gangue calcite mineral (sp.gr 2.7) gravity technique is recommended for recovery of zinc minerals [23,24].

3.3.1. Effect of Inclination Angle

Figure (6) illustrates the relation between inclination angle, grade and recovery of the shaking table at constant water flow rate 25 l/ min, feed rate 150 gm/min, and stroke length 2.5 cm. It is clearly noticed that, with increasing the inclination angle; the grade and recovery increase and reach to the maximum values at the inclination angle 4 degree. At such conditions, the concentrate product has ZnO % and recovery of 62.30% and 92.03% respectively. On the other hand it is noticed that with increasing the inclination angle above 4 degree the grade and recovery are decreased. This is explained according to that the larger the inclination angle, the more difficult for good distribution of particles on the shaking table.

3.3. 2.Effect of Stroke Length (cm)

Figure (7) shows the grade and recovery of zinc at different stroke lengths of shaking table and at constant water flow rate 25 l/ min, feed rate 150 gm/min, and inclination angle 4 degree. It is noticed that good separation occurs at small values of the stroke length. This is due to that, any increase in the stroke length, the more disturbance of the particles occur on the shaking table and hence the more difficult separation. The most efficient stroke length is 2.5 cm; at which a concentrate product with an assay of 60.22% ZnO, and a recovery of 91.12% was obtained.

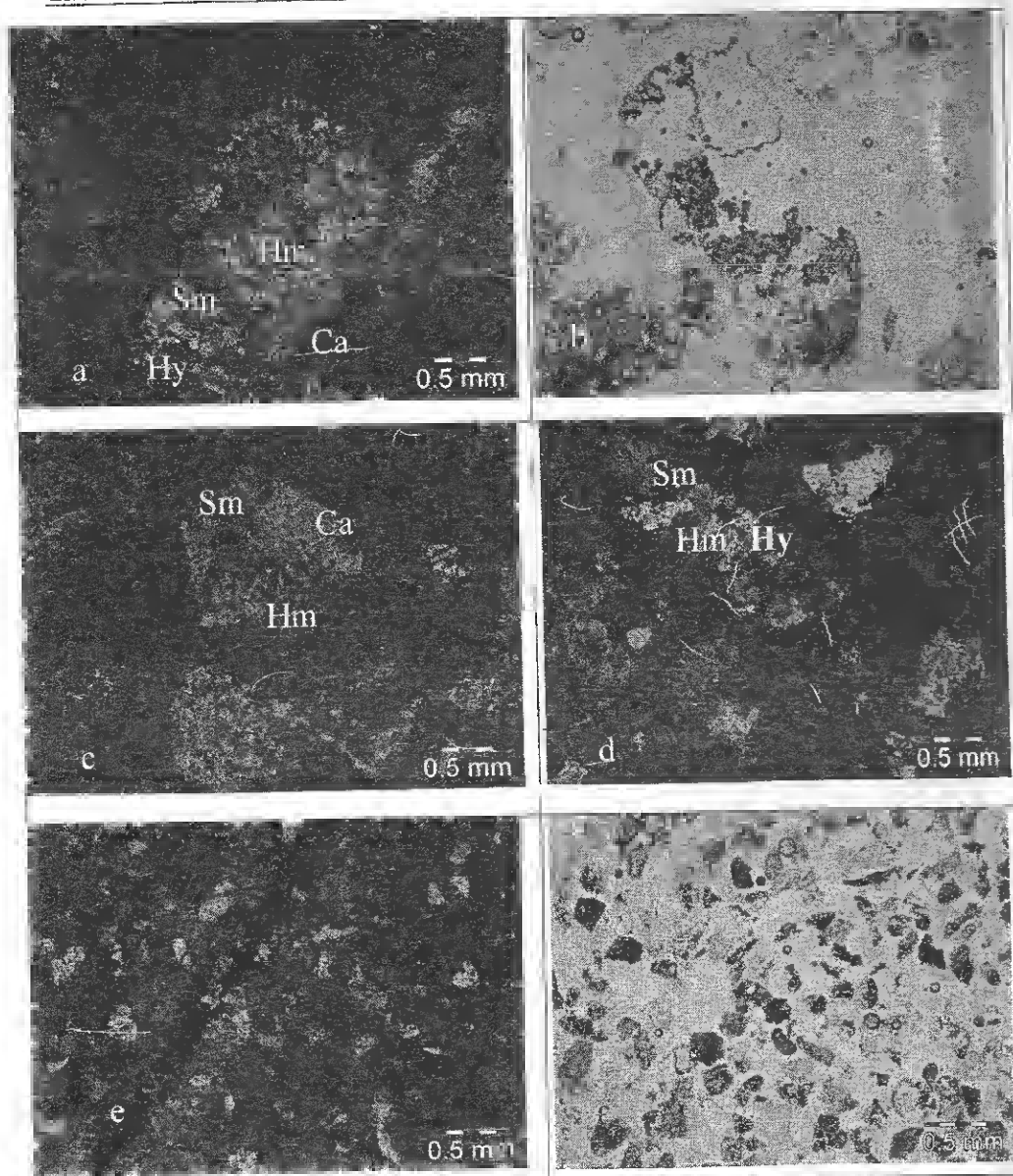


Fig.5. a) 0.833 mm size fraction shows (composite particale) complex interlocking and growth between non-sulphide Zn minerals (smithsonite, hydrozincite and hemimorphite) and calcite gangue minerals, under CN. b) Same photo in a under PPL. c) 0.589 mm size fraction shows ternary particles of smithsonite (sm), hemimorphite (Hm) and calcite (ca). d) 0.417 mm size fraction less complex shows simple binary association of smithsonite (sm), hemimorphite (Hm), hydrozincite (Hy) and calcite (ca). e) 0.106 mm size fraction show that the minerals are separated (free), liberation > 90 %. f) same Photo in e under PPL

3.3.3. Effect of Feed Rate (gm/min)

Figure (8) shows the grade and recovery of zinc as a function of feed rates at constant water flow rate 25 l/ min, inclination angle 4degree, and stroke length 2.5cm. It is obvious that the most efficient feed rate is 150 gm/min; at which the concentrate product has an assay of 62.18% ZnO, and a recovery of 93.8%. On the other hand, it is noticed that with increasing the feed rate over 150 gm/min, both grade and recovery decrease in a great manner. This could be explained due to the larger the feed rate, the more crowding of particles on the shaking table, and hence the more difficult conditions of separation on the shaking table.

3.3.4. Effect of Water Flow Rate (l/ min)

Figure (9) shows the grade and recovery of zinc at different water flow rates and at constant feed rate 150 gm/min, inclination angle 4 degree, and stroke length 2.5cm. It is obvious that the most efficient water flow rate is 25 l/min; at which a concentrate product with an assay of 60.85% ZnO, and a recovery of 90.05% was obtained.

From the obtained results it can be seen that the best operating parameters to obtain a concentrate with high assay and recovery are at inclination angle (4 degree), stroke length (2.5 cm), feed rate (150 gm / min), and water flow rate (25 L / min).

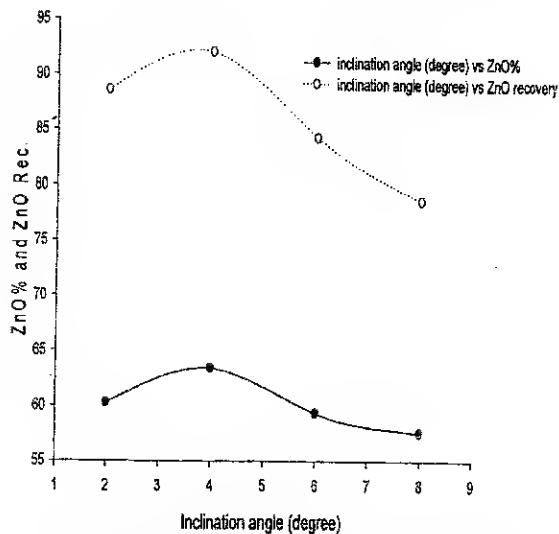


Fig (6) Inclination angle as a function of ZnO% and Recovery, at constant water flow rate= 25 L/min, feed rate= 150 gm/min and stroke length=2.5cm

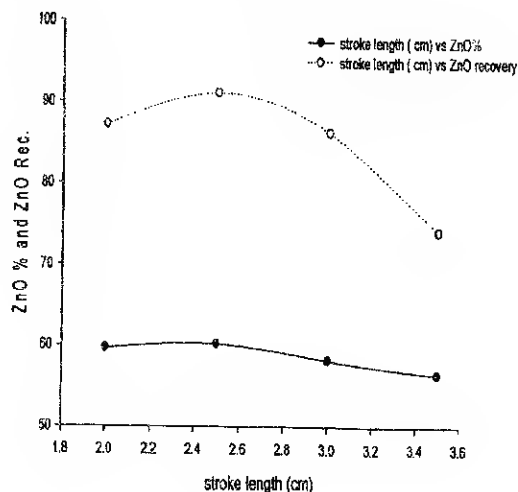


Fig (7) Stroke length as a function of ZnO% and Recovery, at constant water flow rate= 25 L/min, feed rate= 150 gm/min and inclination angle=4 degree

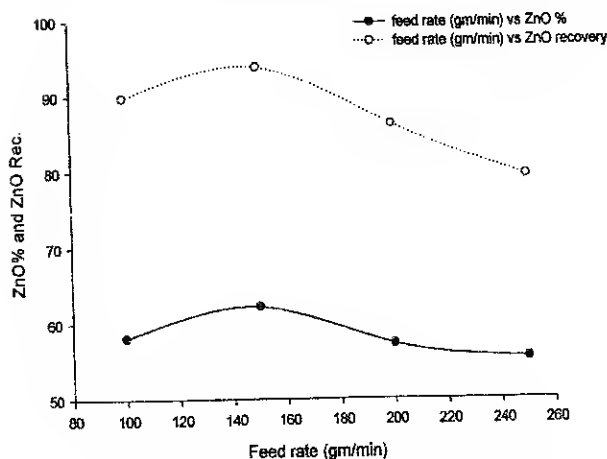


Fig (8) Feed rate as a function of ZnO% and Recovery, at constant water flow rate= 25 L/min, stroke length= 2.5 gm/min and inclination angle = 4°

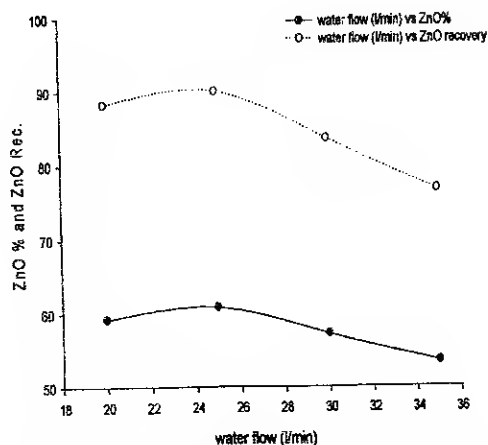


Fig (9) Water flow rate as a function of grade and recovery at constant feed rate= 150 gm/min, stroke length= 2.5 gm/min and inclination angle = 4°

4. CONCLUSIONS

The nonsulfide Zinc mineral association at Um Gheig mine consists mainly of smithsonite, hydrozincite and hemimorphite, which replace both primary sulfide minerals and carbonate host rocks. Calcite and goethite are the main gangue minerals. Smithsonite (ZnCO_3) is the most abundant nonsulfide zinc mineral that occurs in two generations in the studied sample, the first generation of smithsonite, occurs as dull, cryptocrystalline with visible crystals, is finely intergrown with goethite. A late generation of smithsonite occurs as clear rhombohedral crystals. Hydrozincite ($\text{Zn}_5(\text{CO}_3)_2(\text{OH})_6$) is less abundant compared with smithsonite, occurs in different generations in the studied samples as veins, nodule and Botryodial. Hemimorphite $\text{Zn}_4\text{Si}_2\text{O}_7(\text{OH})_2 \cdot \text{H}_2\text{O}$ quite abundant, occurring in at least two generations. A first generation occurs as small concretions with a dusty appearance growing in fine-grained smithsonite. The second one appears as clear elongated crystals growing in veins and cavities.

The experimental beneficiation techniques involved crushing, grinding, and classification to prepare a feed suitable for the separation process. Gravity separation process using "shaking table" was applied to separate the zinc bearing minerals from their associated gangues.

Liberation study indicated that high degree of mineral liberation can be attained at 0.106 mm in size, where individual component are distinctly separated and in turn the shaking table experiments are applied on the feed size of -0.125 +0.080 mm. Four parameters are studied, namely; inclination angle, stroke length, feed rate and water flow rate.

The results show that the optimum parameters of the shaking table to obtain a concentrate of high grade and high recovery are at: inclination angle (4 degree), stroke length (2.5 cm), feed rate (150 gm / min), and water flow rate (25 L / min). At such optimum conditions a grade of 60.85 % ZnO and recovery of 90.05 % can be obtained from a head sample assaying 47.55 % ZnO.

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توصيف وتركيز رواسب الزنك بمنطقة أم غيج بساحل البحر الأحمر

بطرق الفصل الجاذبية

يهدف هذا البحث الى فصل رواسب الزنك بمنطقة أم غيج بساحل البحر الأحمر بمصر عن الشوائب المصاحبة باستخدام طرق الفصل الجاذبية "الترابيزة الهزازة" وذلك من خلال دراسة تأثير العوامل المختلفة التي تؤثر على عملية التركيز للوصول الى الظروف المثلى لعملية الفصل.

تعتبر منطقة أم غيج من أهم المناطق التي تتواجد بها رواسب الزنك بمصر. هذه الرواسب - والتي تمثل جزء من ساحل البحر الأحمر بجمهورية مصر العربية - تسمى "كلامينا" أو "كربونات الزنك" وتتكون من خليط من كربونات الزنك (سميزونايت و هيدروزينكيت) و سيليكات الزنك (هيمومورفيت) بالإضافة الى كميات مختلفة من معادن الرصاص والكالسيت والجوتيت.

أجريت الدراسات المعدنية الشاملة على العينات باستخدام حيود الأشعة السينية (XRD) و طيف الأشعة السينية (XRF) و دراسات بتروجرافية على بعض العينات من منجم أم غيج، و من خلال هذه الدراسات تبين أن معدن الزنك موجود بهذه المنطقة في عدة أشكال مثل معدن السميزونايت (50.74 %)، الهيدروزينكيت (18.78 %) و الهيمومورفيت (14.78 %). هذه الرواسب تكونت عن طريق استبدال الرواسب الأولية و الصخور الكربونية الحاوية. كما وجد أن معدن السميزونايت يتواجد في شكلين أحدهما غير متبلور مخلوط مع أكسيد الحديد والشكل الثاني يتواجد على هيئة بللورات ذو شكل معين تترسب في الفراغات الموجودة بين هذه الرواسب. كما تبين من تلك الدراسات أن الشوائب الموجودة بهذه الرواسب يتكون معظمها من معادن الكالسيت و الجوتيت. أما التحليل الكيميائي لهذه العينة بين أنها تحتوي على 47.50 % أكسيد زنك و 1.55 % أكسيد رصاص و 29.28 % فاقد عند الحرق. كما أجريت دراسة لتحديد درجة التحرر بين رواسب الزنك والشوائب المصاحبة في الحجوم الحبيبية المختلفة الناتجة من عملية التحليل الحبيبي للعينة بهدف إعداد العينة لعمليات التركيز، وقد تبين أن أفضل حجم حبيبي يتم عنده الفصل والحصول على أعلى درجة تحرر بين رواسب الزنك و الشوائب المصاحبة بنسبة تتعدى 90 % هو عند حجم حبيبي 0.106 مم.

كما أظهرت نتائج تركيز الخام بطريقه الفصل بالجاذبية أن الظروف المثلى لعملية الفصل التي عندها يمكن الحصول على ركاز ذو تركيز وعائد استرجاع عالي هي زاوية ميل (4 درجة)، طول المشوار (2.5 سم)، معدل تغذية الخام (150 جم/ق) و معدل تغذية الماء (25 لتر/ق). فعند تطبيق هذه الظروف أمكن الحصول على ركاز به 60.85 % أكسيد زنك وبعاث استرجاع 90 % مقارنة بـ 47.50 % أكسيد زنك في العينة الأصلية.



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مجلة العلوم الهندسية

المجلد ٣٩ العدد رقم ١ - يناير ٢٠١١

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